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**The centre-mode instability of viscoelastic plane Poiseuille flow.** (English) Zbl 1461.76025  
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Summary: A modal stability analysis shows that plane Poiseuille flow of an Oldroyd-B fluid becomes unstable to a ‘centre mode’ with phase speed close to the maximum base-flow velocity,  $U_{\max}$ . The governing dimensionless groups are the Reynolds number  $Re = \rho U_{\max} H / \eta$ , the elasticity number  $E = \lambda \eta / (H^2 \rho)$  and the ratio of solvent to solution viscosity  $\beta = \eta_s / \eta$ ; here,  $\lambda$  is the polymer relaxation time,  $H$  is the channel half-width and  $\rho$  is the fluid density. For experimentally relevant values (e.g.  $E \sim 0.1$  and  $\beta \sim 0.9$ ), the critical Reynolds number,  $Re_c$ , is around 200, with the associated eigenmodes being spread out across the channel. For  $E(1 - \beta) \ll 1$ , with  $E$  fixed, corresponding to strongly elastic dilute polymer solutions,  $Re_c \propto (E(1 - \beta))^{-3/2}$  and the critical wavenumber  $k_c \propto (E(1 - \beta))^{-1/2}$ . The unstable eigenmode in this limit is confined in a thin layer near the channel centreline. These features are largely analogous to the centre-mode instability in viscoelastic pipe flow [*P. Garg et al.*, “Viscoelastic pipe flow is linearly unstable”, *Phys. Rev. Lett.* 121, No. 2, Article ID 024502, 6 p. (2018; doi:10.1103/PhysRevLett.121.024502)], and suggest a universal linear mechanism underlying the onset of turbulence in both channel and pipe flows of sufficiently elastic dilute polymer solutions. Although the centre-mode instability continues down to  $\beta \sim 10^{-2}$  for pipe flow, it ceases to exist for  $\beta < 0.5$  in channels. Whereas inertia, elasticity and solvent viscous effects are simultaneously required for this instability, a higher viscous threshold is required for channel flow. Further, in the opposite limit of  $\beta \rightarrow 1$ , the centre-mode instability in channel flow continues to exist at  $Re \approx 5$ , again in contrast to pipe flow where the instability ceases to exist below  $Re \approx 63$ , regardless of  $E$  or  $\beta$ . Our predictions are in reasonable agreement with experimental observations for the onset of turbulence in the flow of polymer solutions through microchannels.

**MSC:**

76A10 Viscoelastic fluids  
76F06 Transition to turbulence

**Keywords:**

transition to turbulence; viscoelasticity

**Software:**

Differentiation Matrix Suite

**Full Text:** DOI

**References:**

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